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# Pd/C-CeO<sub>2</sub> Anode Catalyst for High Performance Platinum Free Anion Exchange Membrane Fuel Cells

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**Abstract:** One of the biggest obstacles to the diffusion of fuel cells is their cost, a large part of which is due to platinum (Pt) electrocatalysts. Complete removal of Pt is a difficult if not impossible task for proton exchange membrane fuel cells (PEM-FCs). The Anion Exchange Membrane Fuel Cell (AEM-FC) has long been proposed as a solution as non-Pt metals may be employed. Despite this, few examples of Pt free AEM-FCs have been demonstrated with modest power output. The main obstacle preventing the realization of a high power density Pt free AEM-FC is sluggish hydrogen oxidation (HOR) kinetics of the anode catalyst. Here we describe a Pt free AEM-FC that employs a mixed carbon-CeO<sub>2</sub> supported palladium (Pd) anode catalyst that exhibits enhanced kinetics for the HOR. AEM-FC tests run on dry H<sub>2</sub> and pure air show peak power densities of more than 500 mW cm<sup>-2</sup>.

Recent analyses have shown that among PEM-FC components around 45% of the cost comes from the platinum (Pt) electrocatalyst.<sup>[1]</sup> Therefore, a complete removal of Pt from fuel cells and replacement with metals that are less expensive and more abundant in nature is crucial to make this technology an affordable solution for automotive as well as other large scale applications. As an alternative to PEM-FCs that operate under corrosive acidic conditions the use of alkaline anion exchange membrane fuel cells (AEM-FC) may reduce costs by avoiding the use of platinum.<sup>[2]</sup>

In the AEM-FC cathode, non-noble metals can readily replace Pt.<sup>[3]</sup> Varcoe *et al* have recently comprehensively reviewed the range of AEMs and ionomers developed for electrochemical systems, including AEM-FCs.<sup>[4]</sup> Less attention

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has been paid to the anode catalyst for the hydrogen oxidation reaction (HOR).<sup>[2e, 5]</sup> In stark contrast to PEM-FCs, HOR kinetics are quite slow in alkaline media. Indeed, the HOR activity on carbon-supported noble metals (Pt, Pd and Ir) decreases by a factor of ca. 100 when switching from low to high pH.<sup>[6]</sup> Little progress has been made since Lu and co-workers first demonstrated in 2008 a noble-metal-free H<sub>2</sub>/O<sub>2</sub> AEM-FC generating 50 mW cm<sup>-2</sup> peak power at 60 °C,<sup>[5c],23</sup> primarily due to the challenge of overcoming poor HOR kinetics in alkaline media.

In this work, we present a nanoparticle (NP) Pd HOR catalyst with a composite support made of Vulcan XC-72 carbon and CeO<sub>2</sub> (C-CeO<sub>2</sub>) which exhibits enhanced HOR kinetics in alkaline media. Ceria (CeO<sub>2</sub>) was used, as it is one of the most oxygen deficient compounds, known for rapid its saturation with OH<sup>-</sup> ions in alkaline media<sup>[7]</sup> and spillover of OH<sup>-</sup> to supported metal nanoparticles.<sup>[7b]</sup> We have found in previous studies that a mixed ceria-carbon support enhances the activity of Pd anodes in Direct Ethanol Fuel Cells (DEFC) by promoting the transfer of OH<sup>-</sup> to form active Pd<sup>I</sup>OH<sub>ads</sub> species.<sup>[8]</sup>

The mixed support contains 50 wt% CeO<sub>2</sub> and 50 wt% Vulcan XC-72 carbon. Pd (10 wt%) was deposited by chemical deposition and reduction (see SI for synthesis details). The fuel cell anode was prepared using either the new composite Pd/C-CeO<sub>2</sub> catalyst or a homemade reference Pd/C catalyst (C = Vulcan XC-72, 10 wt% Pd).<sup>[9]</sup> The anode Pd loading was 0.3 mg cm<sup>-2</sup>. Silver (Ag) was used as a cathode catalyst with a loading of 3.0 mg<sub>Ag</sub> cm<sup>-2</sup>. Membrane electrode assemblies (MEAs)<sup>[10]</sup> with an active area of 5 cm<sup>2</sup> were tested in AEM-FC single cells (see SI for complete description).<sup>[10b, 11]</sup>

Figure 1 shows the cell performance at 73 °C with air (< 10ppm CO<sub>2</sub>) at the cathode (1.0 slm, 1.0 barg, dew point 73°C) and dry H<sub>2</sub> (0.2 slm, 3.0 barg, 25 °C) fed to the anode.



*Figure 1.* Polarization curves of Pt-free AEM-FCs with Pd/C (red) and Pd/C-CeO<sub>2</sub> (blue) anodes.  $T_{cell}$  = 73 °C. Cathode: air (< 10 ppm CO<sub>2</sub>, 1 slm); anode: dry H<sub>2</sub> (0.2 slm).

The AEM-FC with the Pd/C anode performed modestly reaching a maximum power density of 0.1 W cm<sup>-2</sup> and maximum current density of less than 1 A cm<sup>-2</sup>. The C-CeO<sub>2</sub> supported Pd catalyst reaches a peak power density of 0.5 W cm<sup>-2</sup> at a current density of about 1.5 A cm<sup>-2</sup> and a maximum current density of ca. 3 A cm<sup>-</sup> <sup>2</sup>. Significantly higher fuel cell performance is obtained switching the carbon support for the C-CeO<sub>2</sub> support. The enhancement due to CeO<sub>2</sub> on the HOR activity of Pd was investigated in electrochemical cells. Cyclic voltammograms (CV) recorded with Pd/C and Pd/C-CeO<sub>2</sub> in N<sub>2</sub>-sat 0.1 M KOH are shown in Figure 2a. The peaks for hydrogen adsorption and desorption (UPD) can be readily assigned based on literature data.<sup>[8]</sup> A negative shift in the H<sub>UPD</sub> oxidation peak of ca. 90 mV is seen for the C-CeO<sub>2</sub> supported catalyst relative to the C supported catalyst (Figure 2a). This implies that H is bound less strongly on the surface of Pd supported on C-CeO<sub>2</sub>. A weakening of the metal-hydrogen (M-H) binding energy generally enhances the HOR in alkaline media.<sup>[12]</sup> In fact, the rate-determining step (rds) for HOR at high pH is the oxidative desorption of HUPD.<sup>[12a, 12b]</sup> An increase in the HOR activity of Pd/C-CeO<sub>2</sub> with respect to Pd/C is observed using a rotating disk electrode (RDE) in H<sub>2</sub>-sat 0.1 M KOH (Figure 2b). Pd/C exhibits typically sluggish HOR kinetics reaching the diffusion limited current plateau at 0.5 V (RHE).<sup>[12b, 13]</sup> By contrast, the Pd/C-CeO<sub>2</sub> catalyst reaches the diffusion limited current plateau at ca. 0.25 V.



Figure 2. (A) Cyclic voltammetry of Pd/C and Pd/C-CeO<sub>2</sub> in static N<sub>2</sub>-saturated 0.1 M KOH solution. (B) Steady-state polarization curves of HOR in H<sub>2</sub>-saturated 0.1 M KOH (1600 rpm), (C) Tafel slope analysis obtained in H<sub>2</sub>-saturated 0.1 M KOH at 10 mV s<sup>-1</sup> and 1600 rpm.

Tafel analysis for the HOR is shown in Figure 2c.<sup>[14]</sup> Electrochemical data are also listed in Table 1, including the electrochemically active surface area (ECSA), exchange current densities (i<sub>0</sub>) and the mass activity per gram of Pd (i<sub>0, m</sub>). The HOR exchange current density increases more than 20 fold for the C-CeO<sub>2</sub> supported Pd catalyst relative to Pd/C. Both catalysts have a similar ECSA and Pd NP size distribution (see SI for TEM analysis), so such an increase in the activity can be attributed to electronic effects due to Pd-CeO<sub>2</sub> interactions. The Tafel slopes are also similar suggesting the same HOR mechanism (66-68 mV dec<sup>-1</sup>). Such a range of values indicates that the rds for both catalysts is molecular hydrogen dissociative adsorption (Tafel step).<sup>[12b]</sup>

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#### Table 1 Electrochemical data.

	io	ECSA	Tafel slope	İ0, m
	(mA. cm <sub>Pd</sub> <sup>-2</sup> )	m <sup>2</sup> g <sup>-1</sup> Pd	mV dec <sup>-1</sup>	(A g <sub>Pd</sub> <sup>-2</sup> )
Pd/C	2.7	45	68	1.1
Pd/C-CeO <sub>2</sub>	54.5	43	66	24

High angle annular dark field (HAADF) scanning transmission electron microscopy (STEM) and high-resolution transmission electron microscopy (HR-TEM) were used to study the catalyst morphology. Z-contrast STEM micrographs (Figure 3a) of Pd/C-CeO<sub>2</sub> are shown at various magnifications. The agglomerated CeO<sub>2</sub> structures appear brighter than carbon on the STEM images. Pd NPs are visible only on the carbon part of the sample due to poor resolution between Pd and CeO<sub>2</sub> (mean size of carbon supported NPs 2.0 nm, see SI). Therefore to investigate the Pd distribution over both the carbon and ceria parts of the catalyst we used STEM-EDX (energy dispersive X-ray) elemental map analysis. A representative area of the catalyst is shown in Figure 3b, pointing to a notable accumulation of Pd on the ceriarich regions.



*Figure 3.* (a) STEM micrographs of Pd/C-CeO<sub>2</sub> at different magnifications (scale bars from left to right; 200 nm, 100 nm and 50 nm respectively). (b) STEM image of Pd/C-CeO<sub>2</sub> and related EDX maps for C, O, Pd and Ce respectively (scale bar is 20nm).

Strong Pd-CeO<sub>2</sub> interactions would have a significant effect on the oxidation state of the Pd due to the oxide spillover capacity of ceria that would leave most of the Pd in the oxidized form. To verify this the Pd oxidation state in the Pd/C and Pd/C-CeO<sub>2</sub> catalysts was investigated by X-ray Absorption Spectroscopy (XAS). Spectra were also collected on PdO and on a foil of metallic Pd as standards.[15] In Figure 4a a comparison of the XANES (X-ray Absorption Near Edge Structure) spectra clearly shows that Pd in Pd/C-CeO<sub>2</sub> is mostly oxidized, while in Pd/C the palladium is prevalently in its metallic state. EXAFS (Extended Xray Absorption Fine Structure) analysis was carried out modeling the data with two components, i.e. metallic Pd and PdO. The raw EXAFS data and related Fourier Transforms are shown in Figures 4b and 4c respectively. The EXAFS analysis shows Pd(II) accounts for 87 wt% of the total Pd content in Pd/C-CeO<sub>2</sub> (see SI). This is unusual as carbon supported Pd NPs (ca. 2 nm in diameter) are usually at least 50% metallic.<sup>[16]</sup> As expected, only 17 wt% of PdO was found in the Pd/C system.<sup>[16]</sup> The XAS data therefore shows for the C-CeO<sub>2</sub> supported catalyst that the Pd exists primarily as oxide also confirming that Pd is largely supported on the ceria regions.<sup>[17]</sup> Such a structure not only leads to the weakening of the Pd-H bond but also favors the fast transfer of OH<sup>-</sup> ions from ceria to Pd during catalysis.



**Figure 4.** (a) XAS at the Pd K $\alpha$  edge of Pd/C-CeO<sub>2</sub> and Pd/C (XANES spectra of Pd-foil and PdO standards are also shown), (b) EXAFS data and the related (c) Fourier transforms at the Pd K $\alpha$  edge (transformation range 2.8-13.5 Å<sup>-1</sup>, k<sup>2</sup> weight). Dots represent the experimental data while the continuous lines represent the calculated best-fit data.

In summary, the presence of CeO<sub>2</sub> deposited onto the carbon support of a nanoparticle Pd catalyst leads to a fivefold increase in the anode performance relative to a Pd/C catalyst. A careful morphological analysis attests to a fine dispersion of the Pd nanoparticles accumulated mostly on the ceria part of the catalyst. Such a structure helps to weaken the Pd-H bonds and assists in supplying OH<sub>ad</sub> from oxophilic CeO<sub>2</sub> to the Pd-H<sub>ad</sub> (HOR reaction sites), thus accelerating the overall HOR. A Pt-free AEM-FC using this Pd/C-CeO<sub>2</sub> anode catalyst and a Ag cathode catalyst was tested under dry H<sub>2</sub> and partially filtered ambient air (< 10 ppm CO<sub>2</sub>) supplied to the anode and cathode, respectively. This

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entirely Pt-free AEM-FC produced a peak power density of over 500 mW cm<sup>-2</sup>.

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#### References

- [1] J. S. Spendelow and J.Marcinkoski (2013). DOE Fuel Cell Technologies
   Office Record 13012: Fuel Cell System Cost 2013. Accessed November 16, 2015:
- http://energy.gov/sites/prod/files/2014/03/f11/13012\_fuel\_cell\_system\_cost\_20
   13.pdf.
- 3 [2] a) M. Piana, M. Boccia, A. Filpi, E. Flammia, H. A. Miller, M. Orsini, F. Salusti,
- S. Santiccioli, F. Ciardelli, A. Pucci, J Power Sources 2010, 195, 5875-5881; b)
- J. R. Varcoe, R. C. T. Slade, *Fuel Cells* **2005**, *5*, 187-200; c) Y. J. Sa, C. Park,
- H. Y. Jeong, S. H. Park, Z. Lee, K. T. Kim, G. G. Park, S. H. Joo, Angew Chem Int Edit 2014, 53, 4102-4106; d) D. Dekel, in Encyclopedia of Applied
- 37 *Electrochemistry* (Eds.: G. Kreysa, K.-i. Ota, R. Savinell), Springer New York,
- 38 2014, pp. 33-45; e) D. Dekel, in Encyclopedia of Applied Electrochemistry (Eds.:
- G. Kreysa, K.-i. Ota, R. Savinell), Springer New York, **2014**, pp. 26-33.
- [3] a) Y. Nie, L. Li, Z. D. Wei, *Chem Soc Rev* 2015, 44, 2168-2201; b) G. Wu, P.
   Zelenay, *Accounts Chem Res* 2013, 46, 1878-1889.
- [4] [4] J. R. Varcoe, P. Atanassov, D. R. Dekel, A. M. Herring, M. A. Hickner, P. A.
  42 Kohl, A. R. Kucernak, W. E. Mustain, K. Nijmeijer, K. Scott, T. W. Xu, L. Zhuang, Energ Environ Sci 2014, 7, 3135-3191.
- 43 [5] a) A. Serov, C. Kwak, *Appl Catal B-Environ* **2009**, *90*, 313-320; b) W. C.
- Sheng, H. A. Gasteiger, Y. Shao-Horn, J Electrochem Soc 2010, 157, B1529 B1536; c) S. F. Lu, J. Pan, A. B. Huang, L. Zhuang, J. T. Lu, P Natl Acad Sci
   USA 2008, 105, 20611-20614.
- [6] J. Durst, A. Siebel, C. Simon, F. Hasche, J. Herranz, H. A. Gasteiger, *Energ Environ Sci* **2014**, *7*, 2255-2260.
- [7] a) Z. L. A. Feng, F. El Gabaly, X. F. Ye, Z. X. Shen, W. C. Chueh, *Nat Commun* 2014, *5*; b) T. Skala, F. Sutara, M. Skoda, K. C. Prince, V. Matolin, *J Phys-Condens Mat* 2009, *21*.
- [8] V. Bambagioni, C. Bianchini, Y. X. Chen, J. Filippi, P. Fornasiero, M.
  Innocenti, A. Lavacchi, A. Marchionni, W. Oberhauser, F. Vizza, *Chemsuschem*2012, 5, 1266-1273.
- [9] V. Bambagioni, C. Bianchini, J. Filippi, W. Oberhauser, A. Marchionni, F.
   Vizza, R. Psaro, L. Sordelli, M. L. Foresti, M. Innocenti, *Chemsuschem* 2009, *2*, 99-112.
- [10] a) S. Gottesfeld, D. Dekel, D. S. Simakov (Cellera Inc), US20100216052
   A1, 2010; b) S. Gottesfeld, Z. Gottesfeld, D. Dekel; D.S., Simakov, (Cellera Inc),
   US8257872 B2, 2012.
- [11] a) S. Gottesfeld, D. Dekel, Z. Gottesfeld, D. S. Simakov, (Cellera Inc),
  US8637196 B2, 2014; b) D. G. Dekel, S. Gottesfeld, WO2013184269 A3,
  (Cellera Inc), 2013; c) S. Gottesfeld, D. Dekel, Z. Gottesfeld, S. D. Simakov,
  (Cellera Inc), US7943258 B2, 2011; d) S. Gottesfeld, Z. Gottesfeld, D. Dekel, S.
  D Simakov, Japan 2015-038888, 2014.

[12] a) Y. Wang, G. W. Wang, G. W. Li, B. Huang, J. Pan, Q. Liu, J. J. Han, L. Xiao, J. T. Lu, L. Zhuang, *Energ Environ Sci* **2015**, *8*, 177-181; b) S. St John, R. W. Atkinson, R. R. Unocic, T. A. Zawodzinski, A. B. Papandrew, *J Phys Chem C* **2015**, *119*, 13481-13487; c) W. C. Sheng, Z. B. Zhuang, M. R. Gao, J. Zheng, J. G. G. Chen, Y. S. Yan, *Nat Commun* **2015**, *6*.

[13] M. Shao, J Power Sources 2011, 196, 2433-2444.

[14] P. J. Rheinlander, J. Herranz, J. Durst, H. A. Gasteiger, *J Electrochem Soc* **2014**, *161*, F1448-F1457.

[15] L. Q. Wang, A. Lavacchi, M. Bellini, F. D'Acapito, F. Di Benedetto, M. Innocenti, H. A. Miller, G. Montegrossi, C. Zafferoni, F. Vizza, *Electrochim Acta* 2015, *177*, 100-106.

[16] W. J. Zhou, M. Li, O. L. Ding, S. H. Chan, L. Zhang, Y. H. Xue, Int J Hydrogen Energ **2014**, 39, 6433-6442.

[17] a) W. J. Shen, Y. Matsumura, *J Mol Catal a-Chem* 2000, *153*, 165-168; b)
 Y. Y. Zhou, N. J. Lawrence, T. S. Wu, J. Liu, P. Kent, Y. L. Soo, C. L. Cheung, *Chemcatchem* 2014, *6*, 2937-2946.



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